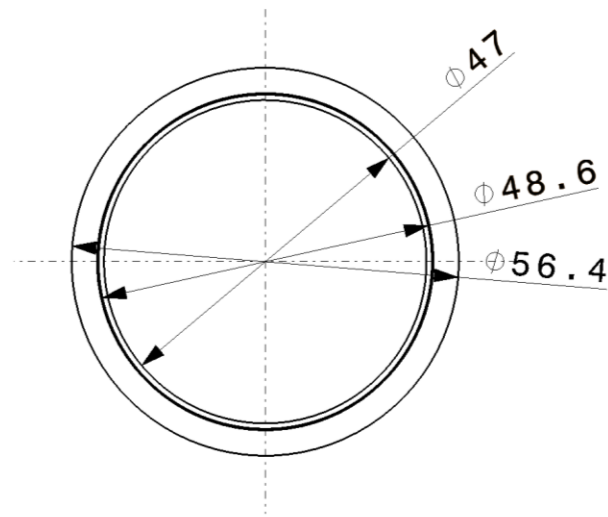


CFD thermal simulations IBL with 47 mm i.d. beam pipe

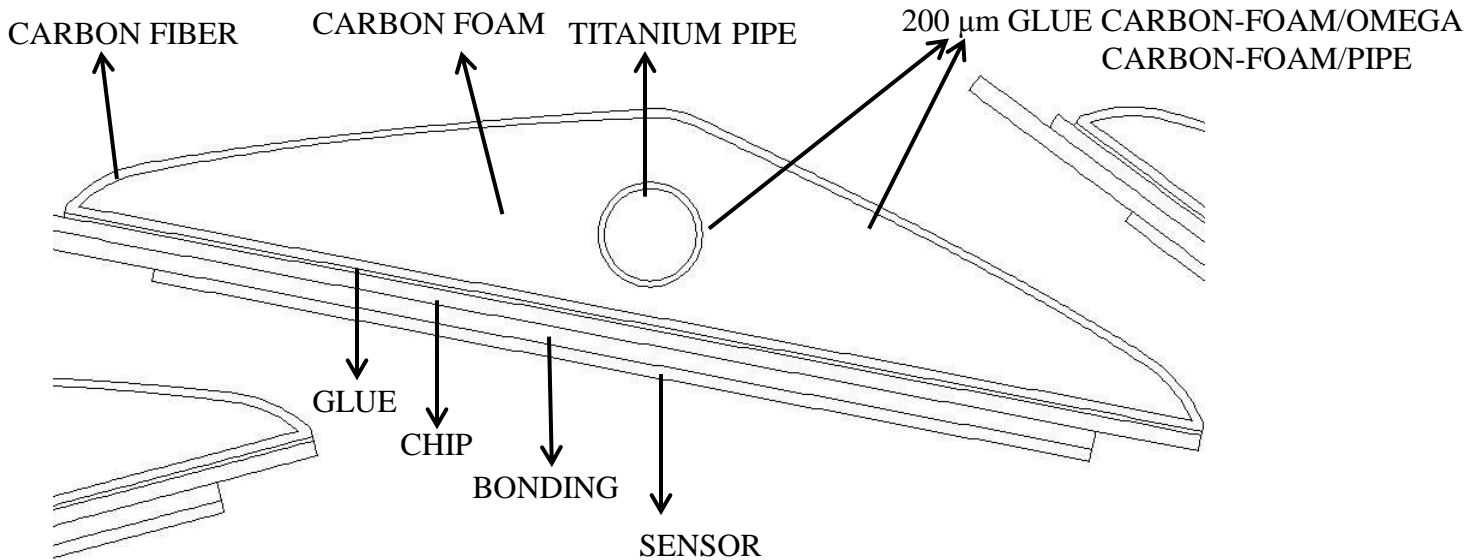
Enrico Da Riva, Anne-Laure Lamure
CFD Team (EN/CV)

Geometry and material properties



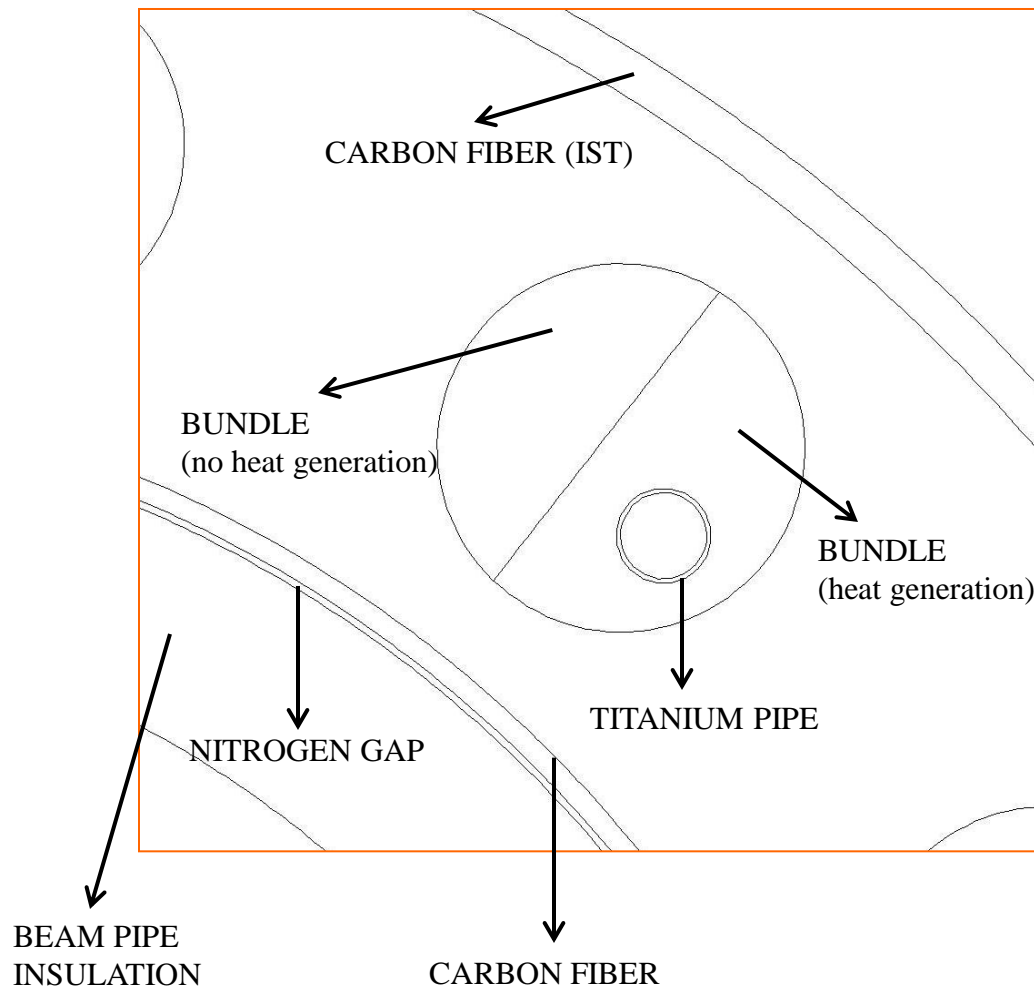
LAYER	POSITION		
-5-	-5-	ALUMINIUM FOIL	: 0.05
-4-	-3-	2 LAYERS POLYIMIDE TAPE (KAPTON)	: 2X0.06
-3-	-4-	AEROGEL INSULATION (COMPRESSED)	: 4
-2-	-3-	2 LAYERS POLYIMIDE TAPE (KAPTON)	: 2X0.06
-1-	-2-	HEATERS	: 0.2
	-1-	ATLAS BEAM VACUUM CHAMBER VI VACUUM TUBE	

- Insulation layer ($48.6 \text{ mm} < D < 56.4 \text{ mm}$) modeled in the CFD simulations.
- Equivalent thermal conductivity $0.0156 \text{ W m}^{-1}\text{K}^{-1}$ (\sim aerogel conductivity).
- Boundary conditions ($250 \text{ }^\circ\text{C}$ for bake out) set at the outside of beryllium pipe.
- Aluminum foil emissivity = 0.05 (slightly overestimated).



MATERIALS		
	Thickness [μm]	Conductivity [$\text{W m}^{-1} \text{K}^{-1}$]
OMEGA (Carbon Fiber)	150	2.2
CARBON FOAM	-	25
TITANIUM PIPE (i.d. 1.5 mm)	100	7.2
GLUE	70	1
CHIP (silicon)	250	148
BONDING	300	6.32
SENSOR (silicon)	200	148

❑ Perfect thermal contact between different layers in the CFD simulations.



MATERIALS	
	Conductivity [W m ⁻¹ K ⁻¹]
CARBON FIBER	2.2
TITANIUM PIPE (i.d. 1 mm)	7.2
BEAM PIPE INSULATION	0.0156
BUNDLE	0.5 - 0.02

- ❑ Difficult estimation of the bundle equivalent thermal conductivity.
- ❑ Two cases considered: full polyimide ($k = 0.5 \text{ W m}^{-1}\text{K}^{-1}$) and *very worst case scenario*: solid with thermal properties of nitrogen ($k = 0.02 \text{ W m}^{-1}\text{K}^{-1}$).

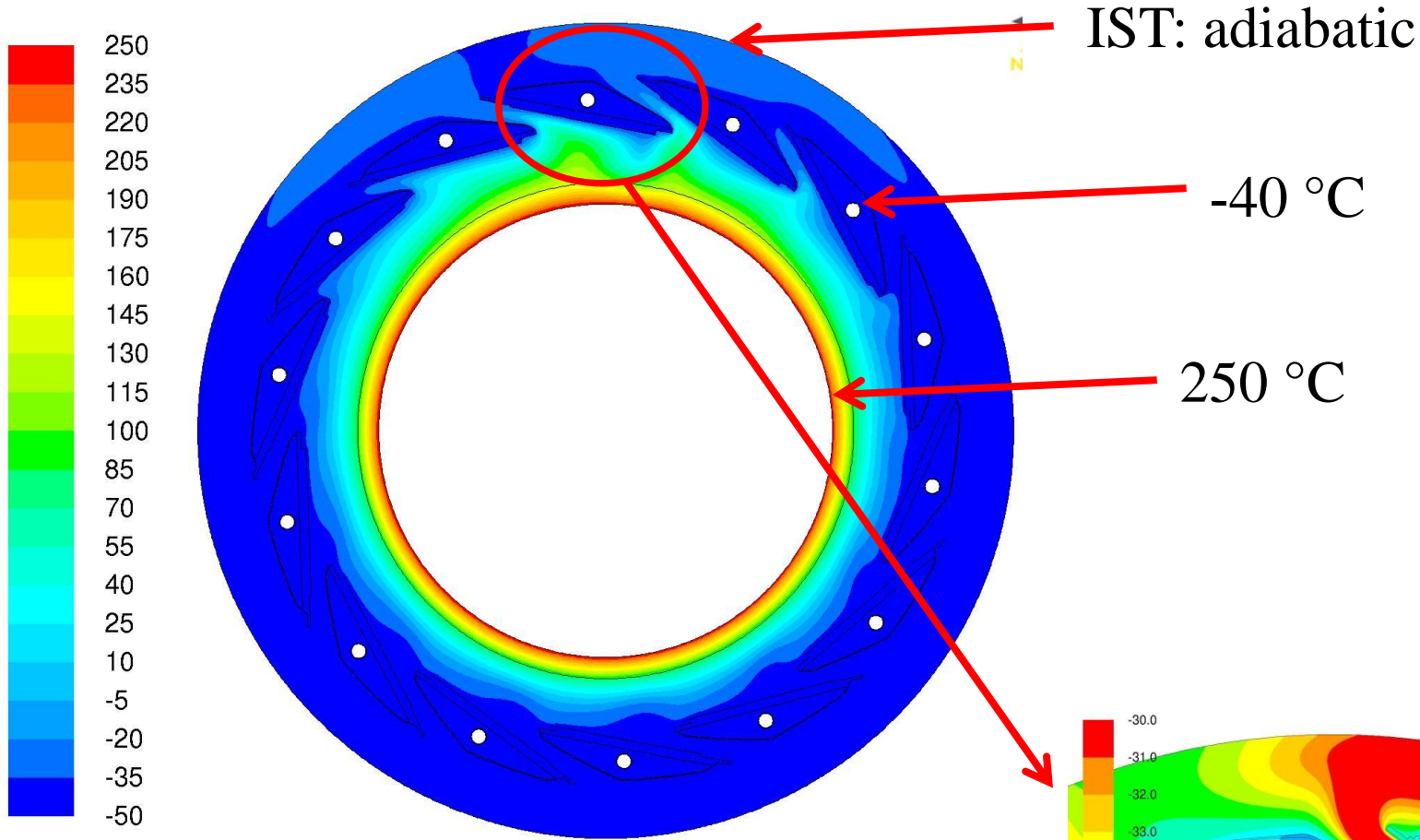
Simulation cases

- 1. IBL-only cross section, bake-out**
- 2. IBL-only cross section, nominal operation**
- 3. Services-only cross section, bake-out**
- 4. Services-only cross section, nominal operation**

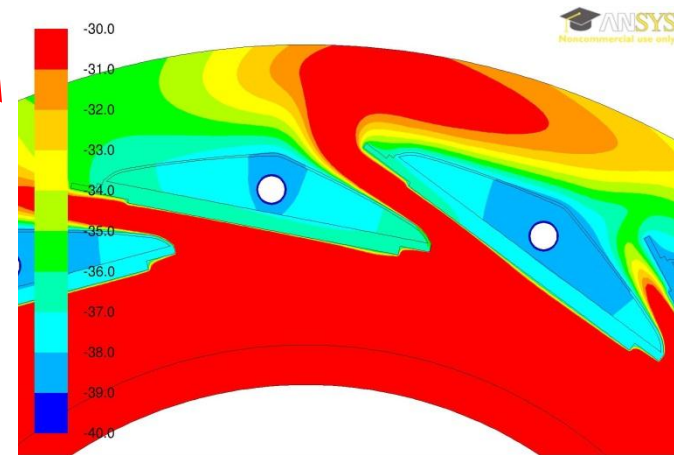
Settings

- Nitrogen flow rate = 0 kg/s.
- Natural convection of nitrogen taken into account.
- Radiative heat transfer taken into account (emissivity 0.05 for beam pipe, 1 for other surfaces).
- Dependence of nitrogen properties on temperature taken into account.
- Laminar natural convection flow.
- Geometry of B-layers not available. IST set as adiabatic.

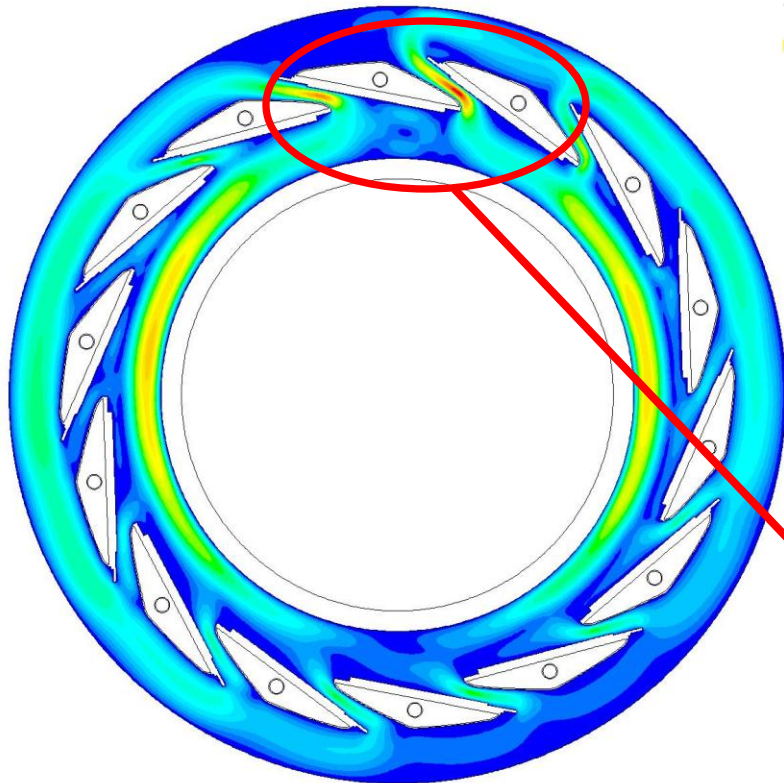
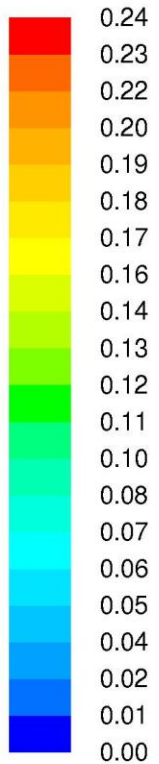
1. IBL-only, bake-out (temperature)



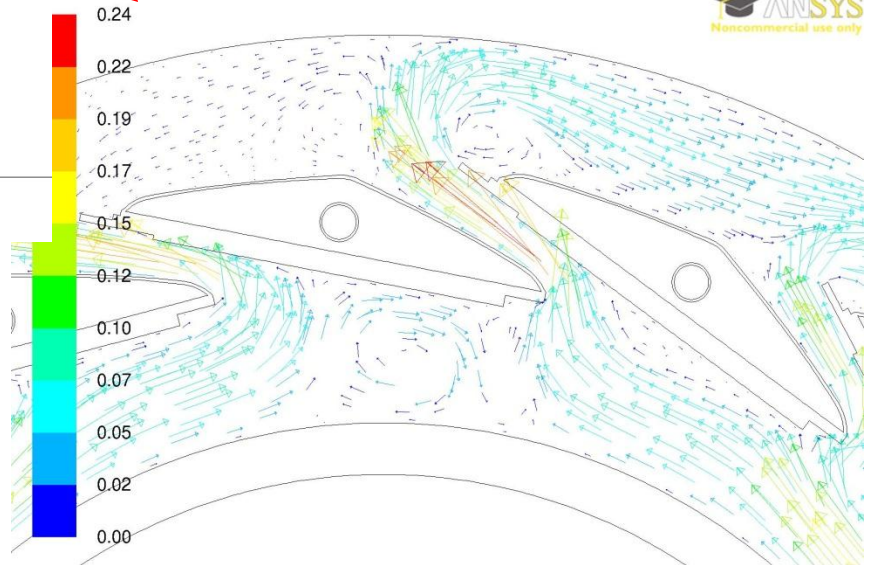
Contours of Static Temperature (c)



1. IBL-only, bake-out (velocity)



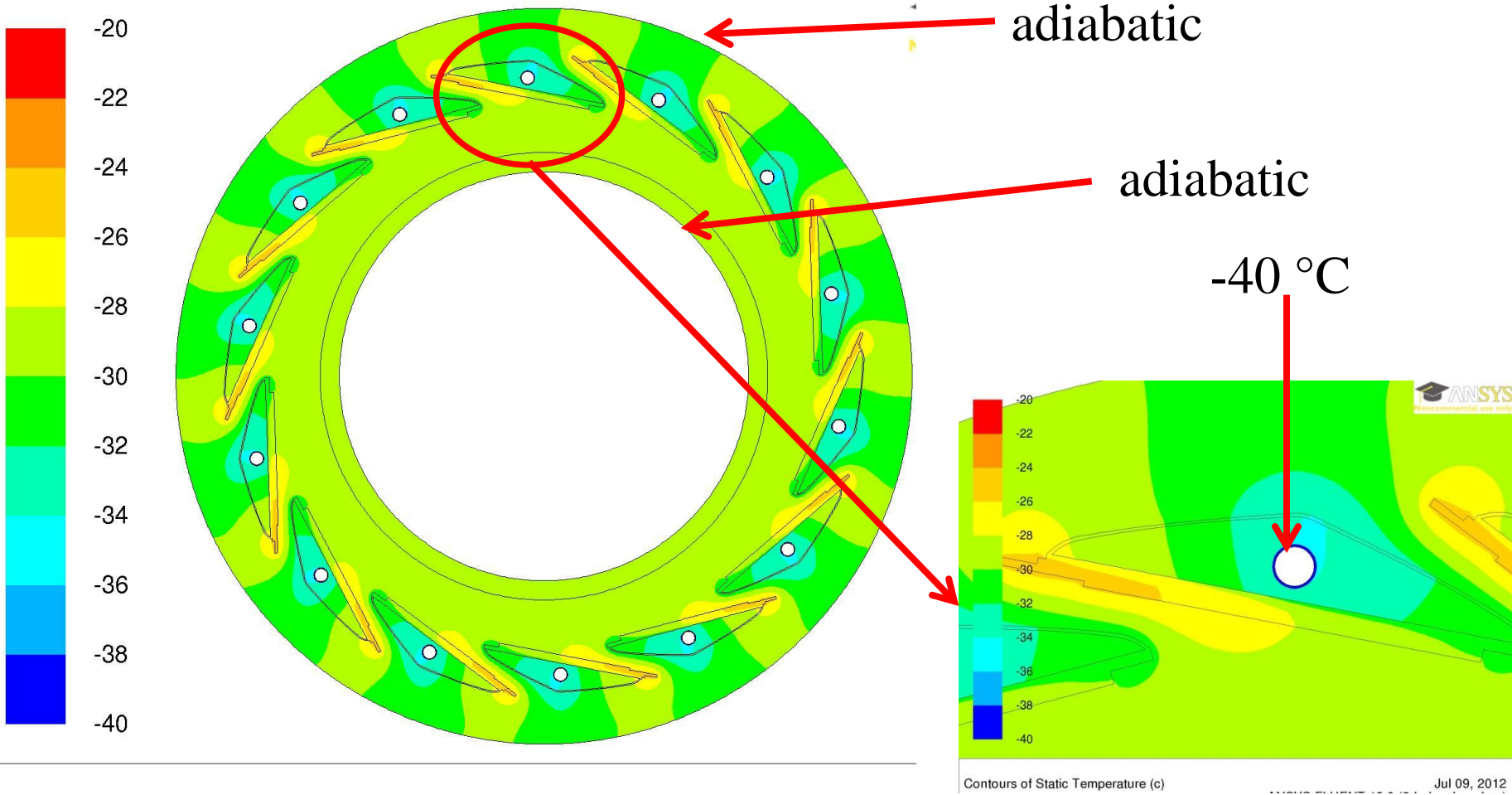
Contours of Velocity Magnitude (m/s)



Velocity Vectors Colored By Velocity Magnitude (m/s)

Jul 09, 2012

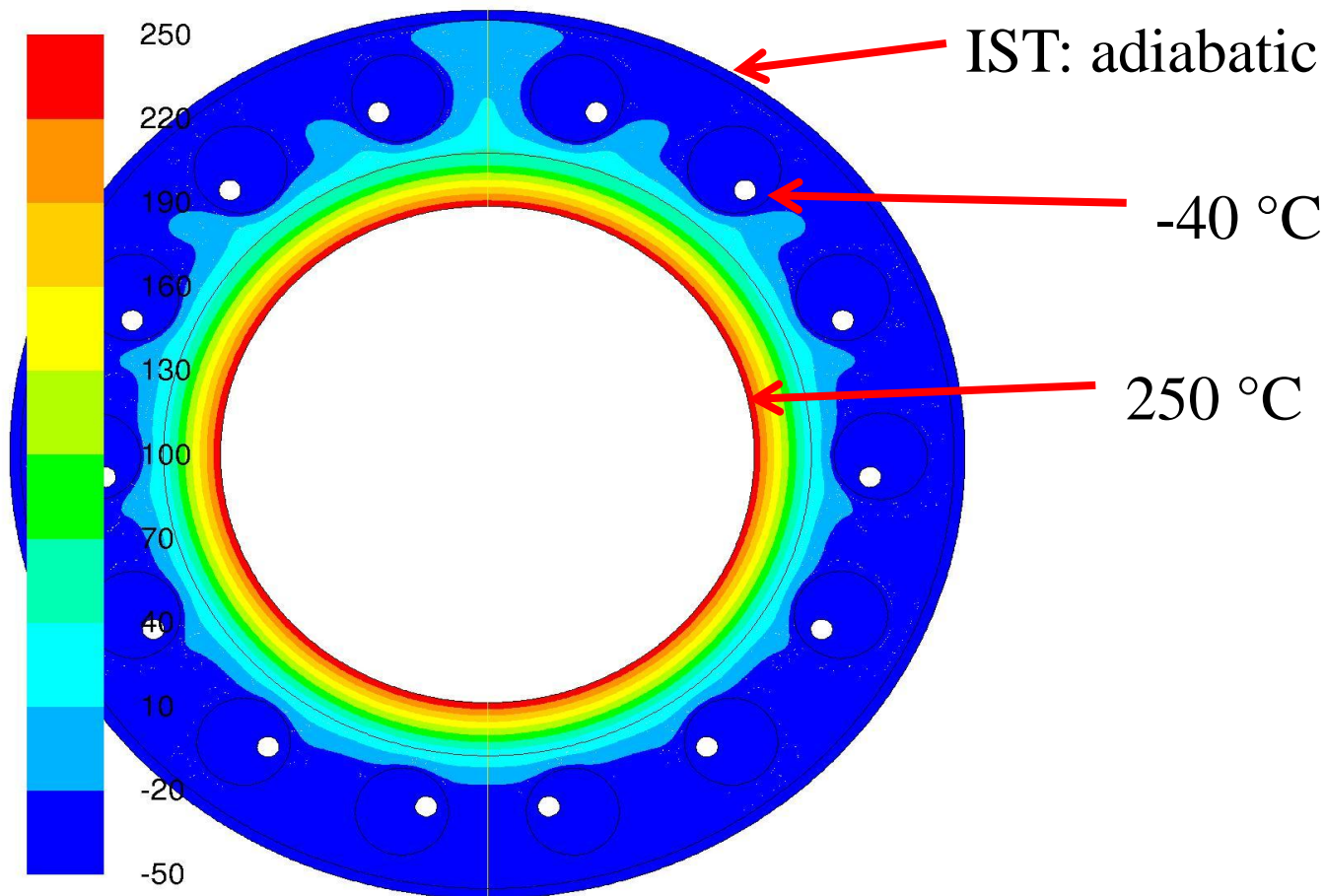
2. IBL-only, nominal operation (temperature)



Contours of Static Temperature (c)

❑ 0.5 W cm^{-2} on the chip, 0.35 W cm^{-2} on the sensor (total $\sim 100 \text{ W}$ per stave).

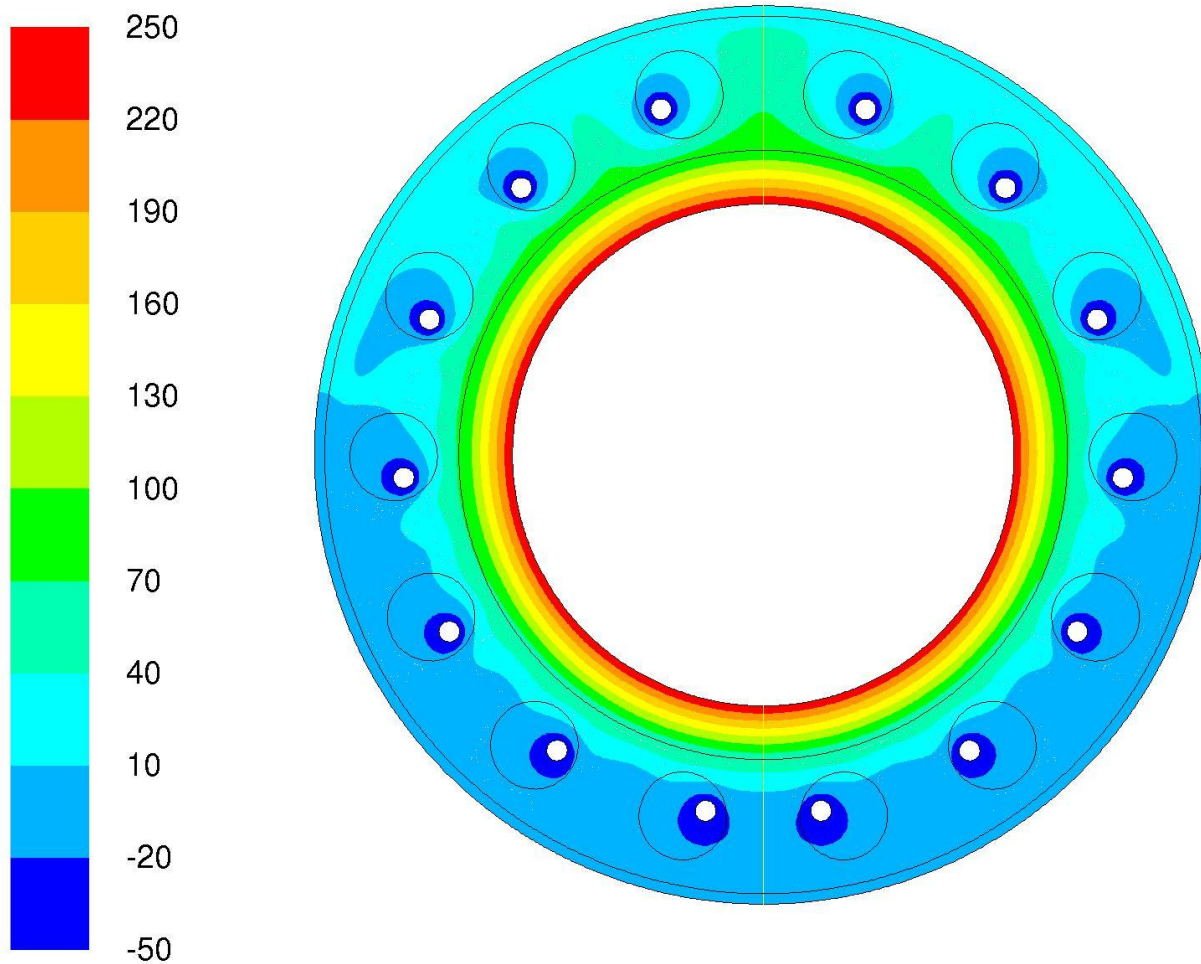
3A) Bundle equivalent conductivity $k = 0.5 \text{ W m}^{-1} \text{ K}^{-1}$



Contours of Static Temperature (c)

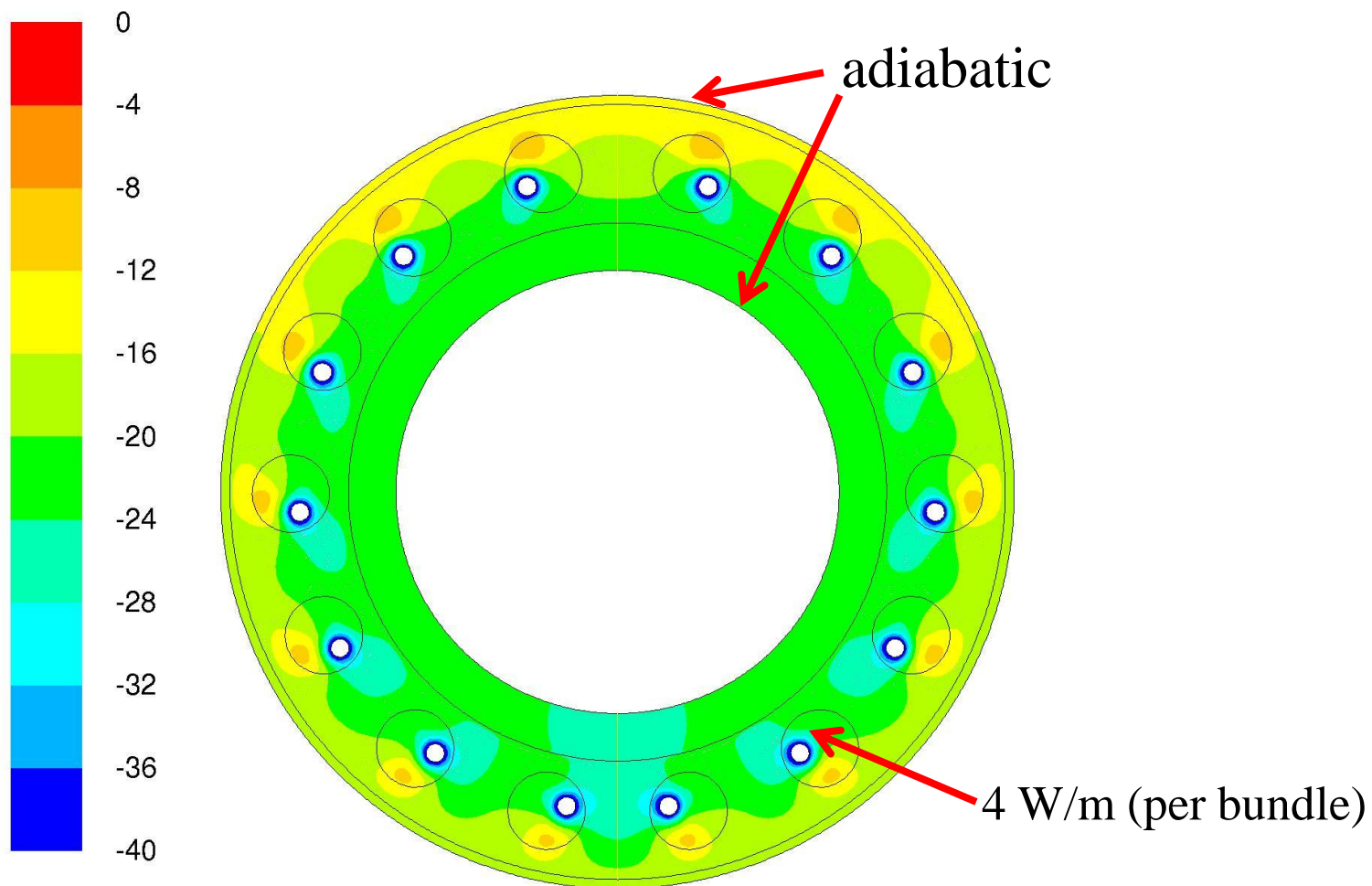
3B) WORST CASE SCENARIO:

Bundle equivalent conductivity $k = 0.025 \text{ W m}^{-1} \text{ K}^{-1}$



Contours of Static Temperature (c)

WORST CASE SCENARIO: Bundle equivalent conductivity $k = 0.025 \text{ W m}^{-1} \text{ K}^{-1}$



Contours of Static Temperature (c)

Summary table

Simulation	T. max (sensor or bundle) [°C]	Heat from beam pipe [W m ⁻¹]	Heat flux on cooling pipe inner surface [W m ⁻²]
IBL, bake-out	-36	167	2532
IBL, nominal operation	-25	0	31850
Services, bake out	-31/48	59/49	1355/1117
Services, nominal operation	<8	0	640

- According to the present results, no cooling problem is expected during the bake-out.

- ❑ In the simulations, the temperature of inner surface of the titanium pipe is set as the CO₂ saturation temperature (i.e. -40°C).
- ❑ A rough estimation of the CO₂ heat transfer coefficient and the actual saturation-to-wall temperature difference has been obtained by means of the Cooper correlation (for pool boiling).

Simulation	Heat flux on cooling pipe inner surface [W m ⁻²]	HTC [W m ⁻² K ⁻¹]	Refrigerant/wall ΔT [K]
IBL bake-out	2532	1400	~2
IBL nominal operation	31850	7400	~4
Services bake out	1355/1117	800	~1.5
Services nominal operation	640	500	~1

Thank you